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B. Surimbayev^{1,2}, L. Bolotova², B. Mishra³, A. Baikonurova¹

¹Satbayev University, Almaty, Republic of Kazakhstan,

²The Branch of the RSE «NC CPMS RK» State Scientific-Industrial Association
of Industrial Ecology "Kazmekhanobr", Almaty, Kazakhstan,

³Worcester Polytechnic Institute, Worcester, USA.

E-mail: surimbaev@gmail.com, L_bolotova@yahoo.com, bmishra@wpi.edu, a.baikonurova@yandex.kz

INTENSIVE CYANIDATION OF GOLD FROM GRAVITY CONCENTRATES IN A DRUM-TYPE APPARATUS

Abstract. Gravimetric, chemical, and mineralogical analyses of a gold-bearing gravity concentrate have been performed. Intensive cyanidation process of the concentrate was carried out in the presence of an organic reagent, while the concentration of sodium cyanide was changed in a drum-type reactor. The use of a reagent activator increased the gold extraction, reduced the time of the reaction, and reduced the leaching losses of gold in to tailings, even when using low concentrations of sodium cyanide.

Keywords: intensive cyanidation, gravity concentration, reagent-activator, gold, leaching.

Introduction. Since the early 1990s, the introduction of centrifugal concentrators, such as Knelson or Falcon concentrators, has significantly increased the percentage of extraction of gold into gravity concentrates by 1-3%, including the processing of ores with a high sulfide content [1-3]. However, standard methods for processing gravity concentrates allow gold recovery at a level of no more than 70% [4]. To solve this problem, intensive cyanidation plants have been tested, which have made it possible to achieve a high extraction of gold from gravity concentrates in an acceptable amount of time for a general technological cycle [5, 6].

The behavior of gold during cyanidation depends on many factors; the main factor is the relationship of gold to ore and rock-forming minerals. Gold can be present in both a free state and in the form of splices with minerals. Any of these conditions can affect the under-extraction of gold during dissolution and can cause an increase in the consumption of reagents. The presence of sulfides in cyanate pulp often inhibits the dissolution of gold, as it tends to form a protective film on the surface of gold. As a result of the oxidation of sulfide minerals in an alkaline solution (pH 10-11) insoluble compounds, such as Ag₂O, FeOOH, CuO, Cu(OH)₂ and Zn(OH)₂ [7-13], can form on the surface of gold. The intensification of the process of gold leaching uses chemical additives to dissolve passivating films of insoluble compounds on the gold surface. However, these additives are expensive and use an increasing concentration of sodium cyanide that ranges from 2–4% [10, 14-16].

The intensive cyanidation of gravity concentrates on an industrial scale has been successfully demonstrated using a drum machine-reactor ILR (Gekko). The drum-type apparatus contains a different prostate device that consists of built ribs, which can improve mass transfer [1, 10].

Therefore, we examined the parameters of intensive cyanidation of gold-bearing concentrate in a drum-type apparatus, along with the addition of a reagent-activator that was based on an aliphatic acid. This process does not require the use of high concentrations of sodium cyanide.

Experimental. The original composition of the gravity concentrate, as determined by an x-ray fluorescence technique on a portable analyzer [Alpha InnovX Systems] shows (in %): Ti – 0.68; Mn – 0.09; Fe – 27.87; Co – 0.15; Cu – 0.16; Zn – 0.04; Pb – 0.05 and Zr – 0.08 as main metals with other

materials adding up to 70.88%. A wet chemical analysis of the gravity concentrate of the major components shows (in %): Cu – 0.11; Zn – 0.025; Fe – 35.02; S_{total} – 32.14; S_{sulphate} – 0.034; and S_{sulfide} – 32.1. The gold content used for research on the gravity concentrate ranged between 77–92 g/t [17], and silver content ranged from 39.7–49.8 g/t. It was previously determined [18, 19] that the gravity concentration and cyanidation of the original ore indicates that the gold is in free form and dissolves easily, which is consistent with the results of optical analysis (figure 1).

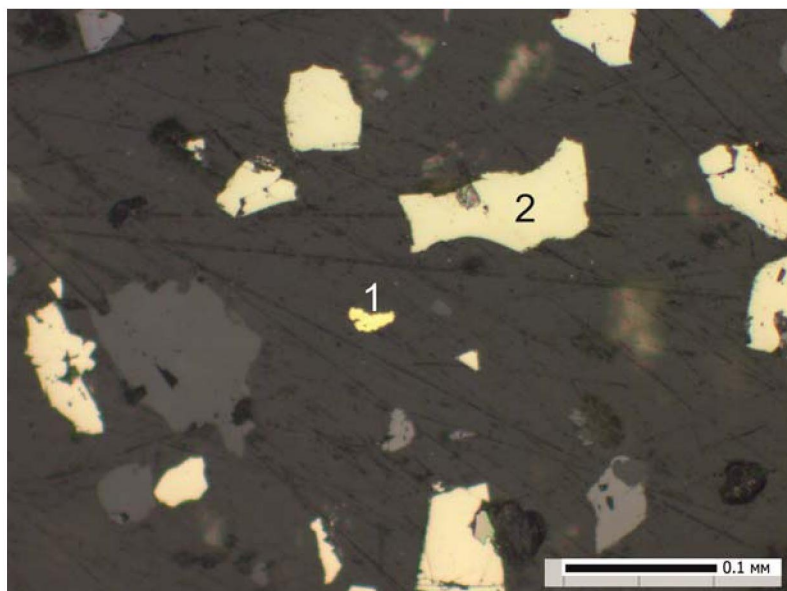


Figure 1 – Micrograph of gravity concentrate: 1 – gold; 2 – pyrite

Through an X-ray diffraction method using an automated diffractometer DRON-3, it was revealed that the concentrate is represented by the following percentages of minerals: pyrite – 78.5; chalcopyrite – 5.5; feldspars – 5.9; and quartz – 10.0. Magnetite, covellite, and iron hydroxides are all present in small quantities (figure 2 and table 1).

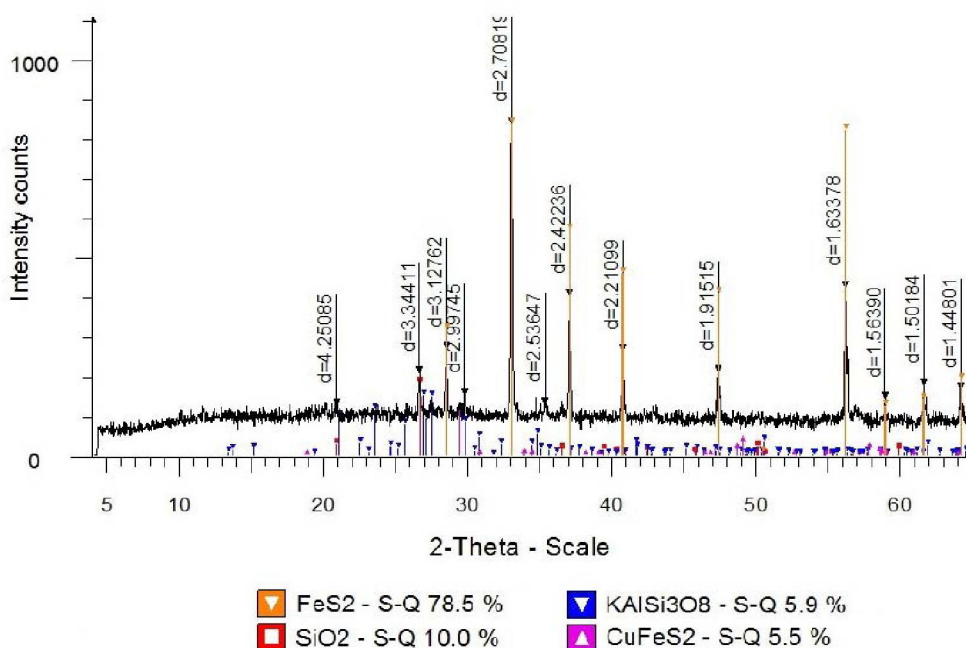


Figure 2 – X-ray diffraction of gravity concentrate

Table 1 – Interplanar distances and phase composition of the gravity concentrate

d-spacing, Å	Rel.int. %	Mineral	Chemical formula
4.25085	15.3	quartz	SiO ₂
3.34411	24.9	quartz	SiO ₂
3.24011	16.6	feldspars	KAlSi ₃ O ₈
3.12762	32.2	pyrite	FeS ₂
3.02968	15.6	chalcopyrite	CuFeS ₂
2.99745	18.4	feldspars	KAlSi ₃ O ₈
2.70819	100.0	pyrite	FeS ₂
2.53647	15.5	magnetite	Fe ₃ O ₄
2.42236	48.2	pyrite	FeS ₂
2.21099	31.5	pyrite	FeS ₂
1.91515	25.2	pyrite	FeS ₂
1.63378	50.7	pyrite	FeS ₂
1.56390	17.2	pyrite	FeS ₂
1.50184	21.2	pyrite	FeS ₂
1.44801	20.0	pyrite	FeS ₂

The results of physico-chemical analysis confirmed that the concentrate mainly consists of sulfide minerals that can form through the dissolution of oxide films on the surface of gold. To destroy the oxide films that passivate the gold surface requires the introduction of special reagent activators under intensive mass-transfer phases.

To achieve this goal, we used a drum apparatus ILR[17], an intensive cyanidation reactor, that simulates industrial installation. The parameters of the drum-type laboratory agitator were as follows: drum diameter, 98 mm; drum length, 214 mm; drum full volume, 1.6 dm³; drum usable volume, 0.38 dm³; and rotation speed of the agitator, 4.25 rpm.

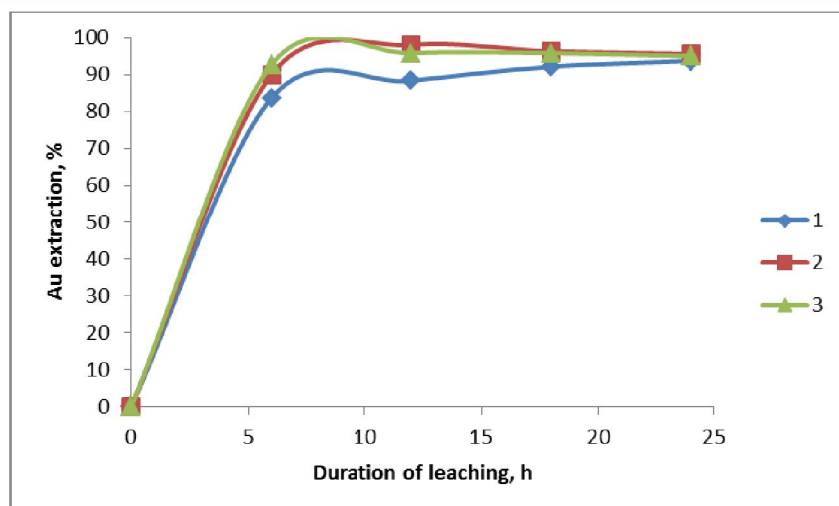
The conditions for leaching of the gold-containing gravity concentrate in the laboratory apparatus were: mass of the gravity concentrate, 0.05 kg; a solid-to-liquid ratio of 1:14; volume of cyanide-containing solution, 0.7 dm³; and a pH of 10.5. As an additive, a reagent activator based on an aliphatic acid with 1.5 and 3.0 kg/t of sodium cyanide was used at a concentration of 0.1, 0.3, and 0.5%.

After the completion of leaching, the filtered solutions were analyzed by atomic-absorption spectroscopy to determine their gold content. Solid phase tailings were washed with water, dried, and were also analyzed for gold content with the assay-gravimetric method.

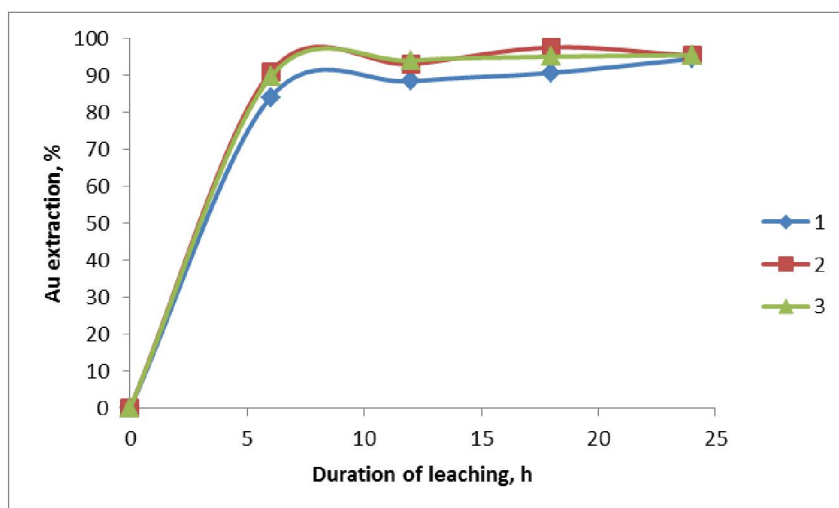
Results and discussion. Figure 3 shows the results of studies on intensive cyanidation of gravity concentrate in a drumtype apparatus.

The data obtained shows that the extraction of gold from the gravity concentrate in a drum-type apparatus, with the addition of a reagent-activator based on an aliphatic acid, was up to 95.5%, while without the addition, it did not exceed 94.5%. It should be noted that in the presence of a reagent-activator, gold dissolves quite rapidly. The duration of the process to dissolve gold is ~12 hours, which shortens the process by more than half of its normal duration.

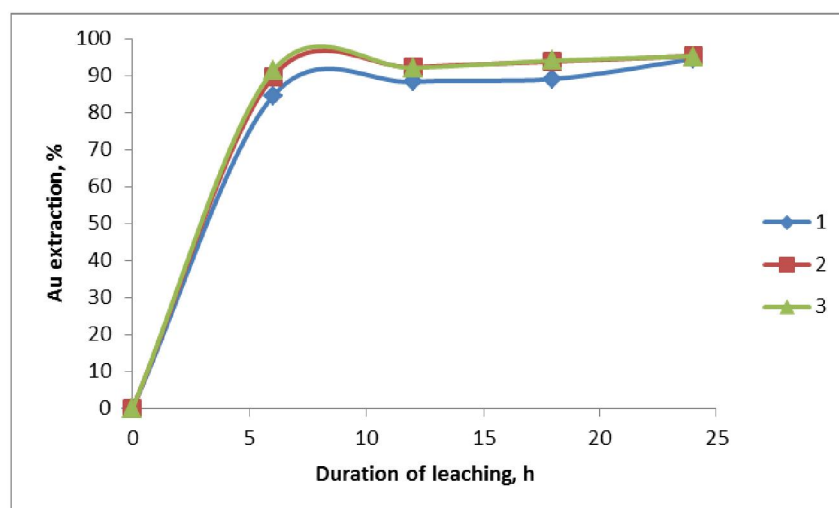
It has been established that the content of gold in tailings after intensive cyanidation by using a reagent-activator falls below 0.5-0.6 g/t, in contrast with the same process without the use of this reagent (table 2).



$C_{NaCN} = 0,1\%$



$C_{NaCN} = 0,3\%$



$C_{NaCN} = 0,5\%$

Figure 3 – Degree of gold extraction in solutions from gravity concentrates.
 Line 1 – without the addition of a reagent-activator; Line 2 – with the addition of a reagent-activator at 1.5 kg/t;
 Line 3 – with the addition of a reagent-activator at 3.0 kg/t

Table 2 – Gold content in the tails after the process of leaching the gravity concentrate

Name of materials	Indicators								
Concentration of NaCN, %	0,1			0,3			0,5		
Content of reagent-activator, kg/t	w/o*	1,5	3,0	w/o	1,5	3,0	w/o	1,5	3,0
Content of gold in tailings, g/t	4,33	3,80	3,90	4,40	3,83	3,85	4,33	3,83	3,70
Note: *w/o – without the addition of a reagent-activator based on an aliphatic acid.									

Conclusion. The data presented show that the use of an effective reagent-activator based on an aliphatic acid as a chemical additive in intensive cyanidation of gold-bearing concentrates in a drumtype apparatus increases gold extraction by 0.7–1.1%, reduces the overall leaching time by half, and reduces the loss of gold with tailings, even when using low concentrations of sodium cyanide.

REFERENCES

- [1] Longley R., McCallum A., Katsikaris N. Intensive cyanidation: onsite application of the InLine Leach Reactor to gravity gold concentrates // *Minerals Engineering*. 2003. Vol. 16. P. 411-419. [https://doi.org/10.1016/S0892-6875\(03\)00054-2](https://doi.org/10.1016/S0892-6875(03)00054-2) (in Eng.)
- [2] Ancia P.H., Frenay J., Dandois P.H. Comparison of the Knelson and Falcon centrifugal separators // In: Richard M. Mozley International Symposium. 1997 (in Eng.)
- [3] Marsden J., House I. *The Chemistry of Gold Extraction*. Society for Mining, Metallurgy and Exploration / 2nd edition. West Sussex, England: Ellis Horwood. 2006. ISBN 10: 0873352408 / ISBN 13: 9780873352406 (in Eng.)
- [4] Laplante A., Staunton W. Pros. 5th Int. Symp.: Hydrometallurgy 2003 // Vancouver, Canada. 2003. Vol. 1. P. 65-74 (in Eng.)
- [5] Dewhirst R.F., Moulton S.P., Coetzee J.A. Intensive cyanidation for the recovery of coarse gold // *Journal of the South African Institute of Mining and Metallurgy*. Vol. 84. 1984. P. 159-163 (in Eng.)
- [6] Davidson J.D., Brown G.A., Schmidt C.G., Hanf N.W., Duncanson, D., Taylor, J.D. The intensive cyanidation of gold-plant gravity concentrates // *Journal of the South African Institute of Mining and Metallurgy*. 1978. Vol. 78. P. 146-165 (in Eng.)
- [7] Karimi P., Abdollahi H., Amini A., Noaparast M., Shafaei S.Z., Habashi F. Cyanidation of gold ores containing copper, silver, lead, arsenic and antimony // *Inter. J. Miner. Process*. 2010. Vol. 95 P. 68-77. <https://doi.org/10.1016/j.minpro.2010.03.002> (in Eng.)
- [8] Dai X., Simons A., Breuer P. A review of copper cyanide recovery technologies for the cyanidation of copper containing gold ores. *Miner. Eng.* 2012. Vol. 25. P. 1-13. <https://doi.org/10.1016/j.mineng.2011.10.002> (in Eng.)
- [9] Deschênes G., Lacasse S., Fulton M. Improvement of Cyanidation Practice at Goldcorp Red Lake Mine // *Miner. Eng.* 2003. Vol. 16. P. 503-509. [https://doi.org/10.1016/S0892-6875\(03\)00079-7](https://doi.org/10.1016/S0892-6875(03)00079-7) (in Eng.)
- [10] Surimbayev B.N., Baikunurova A.O., Bolotova L.S. Prospects for the development of the process of intensive cyanidation of gold-containing products in the Republic of Kazakhstan // *News Natl. Acad. Sci. Repub. Kaz., Ser. Geol. Tech. Sci.* 2017. Vol. 4, N 424. P. 133-141. ISSN 2518-170X (Online), ISSN 2224-5278 (Print). (in Eng.)
- [11] Parga J.R., Valenzuela J.L., Francisco C.T. Pressure Cyanide Leaching for Precious Metals Recovery // *JOM*. 2007. Vol. 59. P. 43-47. <https://doi.org/10.1007/s11837-007-0130-4> (in Eng.)
- [12] Senanayake G. Kinetics and Reaction Mechanism of Gold Cyanidation: Surface Reaction Model via Au (I)-OH-CN Complexes // *Hydrometallurgy*. 2005. Vol. 80. P. 1-12. <https://doi.org/10.1016/j.hydromet.2005.08.002> (in Eng.)
- [13] Ghobadi B., Noaparast M., Shafaei S. Z., Unesi M. Optimization of cyanidation parameters to increase the capacity of Aghdarre gold mill // *JME*. 2014. Vol. 5. P. 121-128 (in Eng.)
- [14] Sandenbergh R.F., Miller J.D. Catalysis of the leaching of gold in cyanide solutions by lead, bismuth and thallium // *Miner. Eng.* 2001. Vol. 14. P. 1379- 1386. [https://doi.org/10.1016/S0892-6875\(01\)00152-2](https://doi.org/10.1016/S0892-6875(01)00152-2) (in Eng.)
- [15] Bayat O., Vapur H., Akyol F., Poole C. Effects of oxidizing agents on dissolution of Gumuskoy silver ore in cyanide solution // *Miner. Eng.* 2003. Vol. 16. P. 395-398. [https://doi.org/10.1016/S0892-6875\(03\)00050-5](https://doi.org/10.1016/S0892-6875(03)00050-5) (in Eng.)
- [16] Surimbayev B., Bolotova L., Baikunurova A., Yesengarayev Ye. Application of chemical additives on leaching gold [Primenenie himicheskikh dobavok pri vyshhelachivani zolota] // *Materials of the International Scientific and Practical Conference «Intensification of hydrometallurgical processes of recycling of natural and technogenic raw materials. Technologies and equipment»*, St. Petersburg, Russia, 2018. P. 294-296. ISBN 978-5-905240-63-8 (In Rus.).
- [17] Surimbayev B., Bolotova L., Baikunurova A., Mishra B. Study on intensive cyanidation of gold from gravity concentrates [Issledovaniya po intensivnomu cianirovaniyu zolota iz gravitacionnykh koncentratov] // *Materials of the International Scientific Conference «Modern problems of complex processing complex ores and technogenic raw materials»*, Plaksin Readings – 2017, Krasnoyarsk, Russia, 2017. P. 273-275. ISBN 978-5-7638-3734-6 (In Rus.).
- [18] Surimbayev B., Baikunurova A., Bolotova L. Studying of the process of gravity concentration of gold-containing ores // *The 49th International October Conference on Mining and Metallurgy*. Bor, Serbia. 2017. P. 160-162. ISBN 978-86-6305-066-2 (in Eng.)
- [19] Surimbayev B., Baikunurova A., Bolotova L. Investigation of the process of gravity concentration of gold-containing sulfide ores [Issledovanie processa gravitacionnogo obogasheniya zolotosoderzhashhih sul'fidnykh rud] // *Reports of the National Academy of Sciences of the Republic of Kazakhstan*, 2017. Vol. 3, N 313. P. 55-60. ISSN 2518-1483 (Online), ISSN 2224-5227 (Print). (In Rus.).

Б. Сүрімбаев^{1,2}, Л. Болотова², Б. Мишра³, Ә. Байқоңырова¹

¹Сәтбаев университеті, Алматы, Қазақстан,

²«ҚР МШКҚӨҰО» РМК Мемлекеттік өнеркәсіптік экология ғылыми-өндірістік бірлестігі филиалы
«Қазмеханообр», Алматы, Қазақстан,

³Вустер политехникалық институты, Вустер, АҚШ

БАРАБАН ТИПТЕС ҚҰРЫЛҒЫДА ГРАВИТАЦИЯЛЫҚ КОНЦЕНТРАТТАН АЛЫНҒАН АЛТЫНДЫ ҚАРҚЫНДЫ ЦИАНИРЛЕУ

Аннотация. Алтынқұрамды гравитациялық концентратта пробирді-гравиметриялық, химиялық және минералдық талдау әдістері жүргізілді. Барабан типтес құрылғыда гравитациялық концентратты қарқынды цианерлеу үрдісі бойынша зерттеу жұмыстары жүргізілді. Қарқынды цианирлеу үрдісін натрий цианидінің концентрациясының өзгеруімен алифаттық қышқылға негізделген органикалық реагентті қолдану арқылы жүргізілді. Жұмыс нәтижесі бойынша, гравитациялық концентратты қарқынды цианирлеуде реагент-активаторды қолдану арқылы алтынды өндіру мөлшері ұлғайтылатыны, байыту уақытын қысқартылатыны, сонымен қатар натрий цианидінің төмен концентрациясын пайдаланған кезде алтынның қалдықтармен жоғалуы азаятыны анықталып көрсетілді.

Түйін сөздер: қарқынды цианирлеу, гравитациялық концентрат, реагент-активатор, алтын, байыту.

Б. Сүрімбаев^{1,2}, Л. Болотова², Б. Мишра³, А. Байқоңырова¹

¹Satbayev University, Алматы, Казахстан,

²Филиал РГП «НЦ КПМС РК» Государственное научно-производственное объединение
промышленной экологии «Казмеханообр», Алматы, Казахстан,

³Вустерский политехнический институт, Вустер, США

ИНТЕНСИВНОЕ ЦИАНИРОВАНИЕ ЗОЛОТА ИЗ ГРАВИТАЦИОННЫХ КОНЦЕНТРАТОВ В АППАРАТЕ БАРАБАННОГО ТИПА

Аннотация. Проведены пробирно-гравиметрические, химические и минералогические анализы золотосодержащего гравитационного концентрата. Проведены исследования по интенсивному цианированию гравитационного концентрата в аппарате барабанного типа. Процесс интенсивного цианирования проводили в присутствии органического реагента на основе алифатической кислоты при изменении концентрации цианида натрия. Показано, что использование реагента-активатора при интенсивном цианировании увеличивает извлечение золота, сокращает время выщелачивания, а также снижает потери золота с хвостами даже при использовании низкой концентрации цианида натрия.

Ключевые слова: интенсивное цианирование, гравитационный концентрат, реагент-активатор, золото, выщелачивание.

Information about the authors:

Bauyrzhan Surimbayev – PhD student, Satbayev University, Satpayevstr 22a, Almaty, Kazakhstan; Research scientist, laboratory of precious metals, The Branch of the RSE «NC CPMS RK» State Scientific-Industrial Association of Industrial Ecology "Kazmekhanobr", 67b, Jandosovstr, Almaty, Kazakhstan; surimbaev@gmail.com; <https://orcid.org/0000-0002-3988-8444>

Lyudmila Bolotova – Candidate of Chemical Sciences, Head of the laboratory of precious metals, The Branch of the RSE «NC CPMS RK» State Scientific-Industrial Association of Industrial Ecology «Kazmekhanobr», 67b, Jandosovstr, Almaty, Kazakhstan; L_bolotova@yahoo.com; <https://orcid.org/0000-0003-0828-9817>

Brajendra Mishra – Ph.D, professor, Worcester Polytechnic Institute, Worcester, Massachusetts, USA; bmishra@wpi.edu; <https://orcid.org/0000-0001-7897-1817>

Aliya Baikonurova – Doctor of Technical Sciences, Professor, Satbayev University, 22a, Satpayevstr, Almaty, Kazakhstan; a.baikonurova@yandex.kz